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Department of Mathematics

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Declaration

I declare that this is my own work and that I have not used any other sources or resources in preparing this work.

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1 Introduction

The migration of contaminants or reactants through porous media is of critical importance for a wide variety of scientific and industrial processes. This process can include both reaction with and without the porous media.¹ Contamination of soils and sands for example, by liquid pollutants can result in those pollutants entering groundwater systems, thus increasing the chance of harm to crops and ecosystems, and water supplies to the public. It is important therefore to characterise such phenomena, and be able to predict the fate of such species, dependent on porous media and pollutant type, over a wide range of conditions. It is known that the nonlinear adsorption of unreactive pollutants can be classified into slow, fast or superfast diffusion, dependent on the characteristics of the diffusion coefficient in the porous medium equation. The diffusion coefficient is often dependent on the saturation level of the contaminant species in the porous medium, which drives the diffusion. This changes over time as the solution

1.1 Background to diffusion through porous media

is the porous medium equation (PME) in 1D Cartesian coordinates. It can be generally stated as

$$\frac{\partial u}{\partial t} = \frac{\partial}{\partial x} \left(D(u(x(t); t)) \frac{\partial u}{\partial x} \right) + s(x);$$

where $D(u(x(t); t))$ is the diffusion coefficient (which, when $D(u) = u^m$, is the PME).

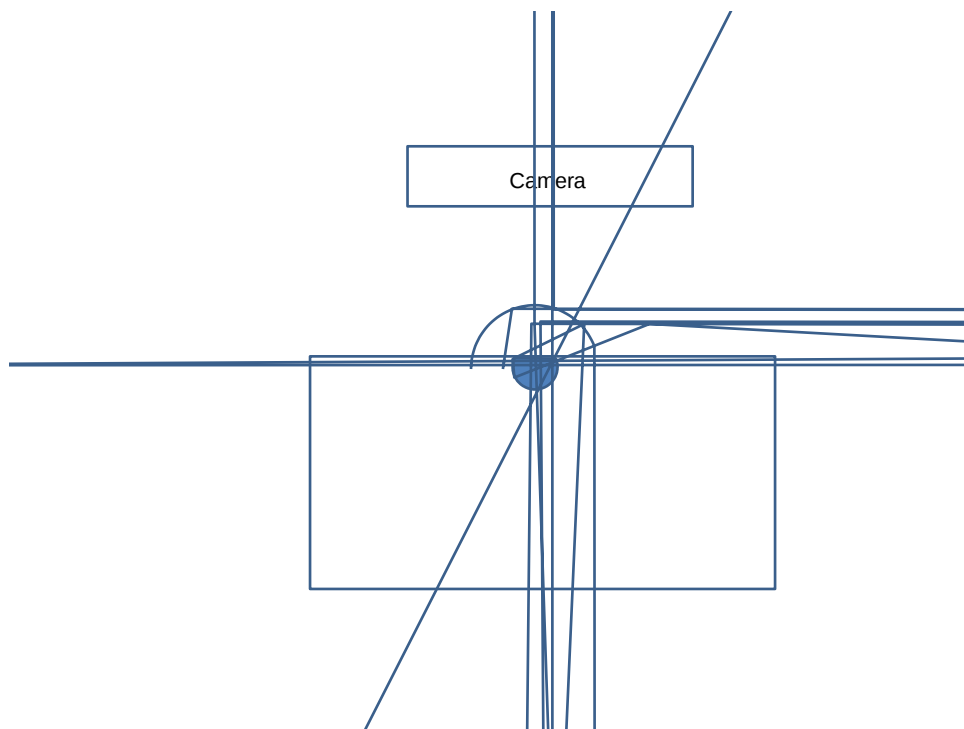
For radial diffusion, the nonlinear PME is given by

$$\frac{\partial u}{\partial t} = \frac{1}{r^{d-1}} \frac{\partial}{\partial r} \left(u^m r^{d-1} \frac{\partial u}{\partial r} \right) + s(r); \quad (1)$$

where d is the number of dimensions. In this study we take $d = 2$. For both radial and cartesian coordinates $s(x(t))$ and $s(r(t))$ represent a source or sink term, such as ingress of another source of liquid into the system, or evaporation of the liquid out of the system respectively. In the case of this study, we do not consider any source or sink terms, particularly since we assume that our migrating liquid is a non reacting, non volatile liquid.

The transition of transport through porous media is very much dependent on the saturation level of the solvent. This change in diffusion behavior can be very sharp as detailed in the study by Lukyanov et al [2]. This transition is seen to occur at about 20% saturation for low saturation levels. The general classification of the "speed" of non linear diffusion with respect to the value of m (142 11.9551 Tf 2249375 and $m(d) = 0.902$)

for slow ($m = 1$) and superfast ($m = 3/2$) diffusion. Where the concentration $u(r)$ is greater than 20% of $u(r = 0)$, for $m = 1$, we present a self similar/analytic solution for $u(r(t); t)$, which is used to obtain the boundary values of the velocity $\frac{dr}{dt}$, rate $\frac{du}{dt}$ and gradient $\frac{du}{dr}$.



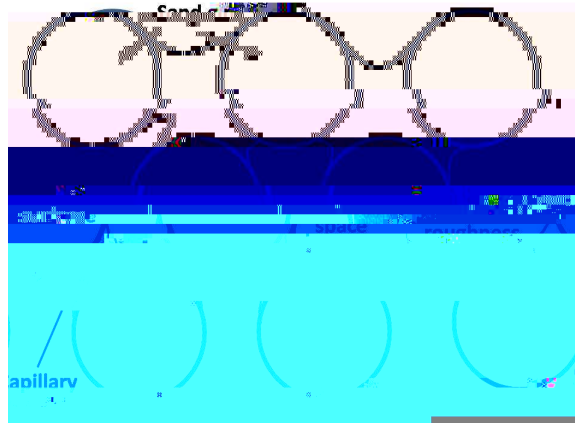


Figure 3: Structure of capillary areas between sand particles at saturation levels greater than 10%

This paper provided evidence, from an environmental pollution perspective, that small concentrations of harmful solvents can travel long distances through packed soils/sands over long periods of time, thus justifying the requirement to investigate the migration of harmful contaminant species.

The transport of liquid through the porous media was deduced to be due to capillary action at the surface-roughness scale of the individual particles, and indeed the total saturation of the sand is the interplay between that within the capillary bridges, and that in the surface roughness around the particles. Generally, the flow obeys a Darcy-like Law, where permeability is related to the geometry of the grooves [4]. In macroscopic modelling of the migration of the nonvolatile liquid, it was assumed that the particles were perfect spheres, and that the wetted grooves within the surface roughness of the particles were completely filled. Modelling results were then compared

following non-dimensionalisation, for saturation, distance and time. When comparing to equation (1), $n = m + 1$. This is known as superfast diffusion. In the standard porous medium equation (which we will use for the slow section of our model), where $m > 1$ in equation (3), the low saturation levels at the edge of the liquid delay the onset of the wetting front, however (and in our model for superfast diffusion), for superfast regimes, the velocity of the wetting front decreases over time as the saturation level/concentration decreases. The results of the model are in agreement with experiment, and for the characterised system with the organic solvent, trioctyl-phosphate (TEHP) at low concentration (deposited on well characterised sand) the superfast diffusion regime is said to hold for $0.5\% < s < 10\%$. It was also shown that the wetted volume, V , fell on a power law with time, where $V \propto t^{0.75}$ as shown in Figure 4.

occur where the solution value for concentration (or saturation) is 20% of its maximum value. As expected, the central node will not move, however, the other nodes in the mesh will move with a velocity that changes with time. This is a first attempt at

In Chapter 4 we present the results of the moving mesh methods for both slow and superfast diffusion in isolation for 2D radial diffusion, followed by the results for the combined numerical method. In the case of the slow diffusion we show the results for constant mass between spatial nodes. We discuss the stability and limitations on the discretisation of time via a Lagrangian type Courant-Friedrichs-Lewy (CFL) condition [7]. This condition prevents the spatial nodes from overtaking one another.

In Chapter 5 we draw some conclusions from the results, comparing the behaviour of the slow and superfast regimes in isolation with the combined diffusion moving mesh scheme.

In Chapter 6 we make recommendations for future study.

2 Generation of an analytic solution for slow diffusion

In this chapter we look for an analytic solution to the porous medium equation where $m = 1$, by generating a self similar solution. We shall firstly describe the scale invariance applied to 2D radial diffusion, and follow this with the generation of the self similar/analytic solution. This method is discussed in reference [8], and adopted in 1D Cartesian coordinates, where $n = 4$, in reference [9].

2.1 Scale invariance for slow diffusion

We consider the case where $m = 1$ and $d = 2$ in the nonlinear porous medium equation (2)

$$\frac{\partial u}{\partial t} = \frac{1}{r^{d-1}} \frac{\partial}{\partial r} r^{d-1} u^m \frac{\partial u}{\partial r} \quad (2)$$

where d is the number of dimensions. We now apply a scaling transformation to equation (2),

$$u = \hat{u}; \quad t = \hat{t}; \quad r = \hat{r}; \quad (3)$$

using the scaling parameter, λ , where α and β are constants. This transforms equation (2) into the new non-dimensionalised variables $\hat{u}$, $\hat{t}$, and $\hat{r}$;

$$-\frac{\partial \hat{u}}{\partial \hat{t}} = \frac{\lambda^{2-\alpha}}{\hat{r}^{d-1}} \frac{\partial}{\partial \hat{r}} \hat{r}^{d-1} \hat{u}^m \frac{\partial \hat{u}}{\partial \hat{r}}$$

and

$$u(b) = 0 \quad \text{at the boundary } r = b(t):$$

This results in

$$\frac{\partial}{\partial t} \int_0^{b(t)} r^{d-1} u \, dr = 0;$$

and so

$$\int_0^{b(t)} r^{d-1} u \, dr = k; \quad (6)$$

where k is a constant. Upon transformation of equation (6) into $\hat{\alpha}$, $\hat{t}$ and $\hat{r}$ we obtain

$$\int_0^{\hat{b}(t)} \hat{r}^{d-1} \hat{u} \, d\hat{r} = k;$$

thus generating a second equation in $\hat{r}$ and $\hat{t}$,

$$\frac{\partial}{\partial \hat{t}} \int_0^{\hat{b}(t)} \hat{r}^{d-1} \hat{u} \, d\hat{r} + 2 \hat{u} \hat{r} = 0; \quad (7)$$

Therefore, solving equations (5) and (7)

$$\hat{u} = \frac{1}{4}; \quad \text{and} \quad \hat{r} = \frac{1}{2};$$

This results in a scale transformation

$$u = \frac{1}{2} \hat{u}; \quad t = \hat{t}; \quad \text{and} \quad r = \frac{1}{4} \hat{r};$$

so

$$\frac{u^{1=}}{\hat{u}^{1=}} = \frac{t}{\hat{t}} = \frac{r^{1=}}{\hat{r}^{1=}};$$

An in depth text on scaling methods and self similarity can be found in reference [11].

2.2 Generation of a self similar solution for slow, nonlinear diffusion

We now introduce two variables, $\hat{u}$ and y , that are independent of $\hat{r}$, and which are invariant under transformation equation (3). We then make $\hat{u}$ a function of y , and then transform as follows

$$\hat{u} = \frac{u}{t} = \frac{\hat{u}}{\hat{t}};$$

$$y = \frac{r}{t} = \frac{\hat{r}}{\hat{t}}:$$

With

where d is a constant of integration. Therefore

$$= A \frac{y^2}{8};$$

where A is a constant. We we can write

$$= A \frac{y^2}{8}; \quad \frac{y^2}{8} \quad A:$$

$$= A \frac{y^2}{8} + :$$

Figure 5 illustrates the self similar solution, equation (8) where $A = 2$, for the original non-linear 2D equation (2), where $d = 2$, $m = 1$. Four time steps are shown. It can be seen that the profile gradually attenuates over time and is symmetric about $r = 0$. In this study we take the initial time,

$$= r u \frac{\partial u}{\partial r} \bigg|_{r_A(t)}^{r_B(t)} + u r \frac{dr}{dt}$$

Algorithm for slow diffusion alone with mass conservation

Initially:

1. Define the initial condition everywhere to be

$$u(r) = 2 - \frac{r^2}{8} \quad \text{at } t_0 = 1$$

2. Discretise the mesh $r_i(t) = r_0(t) + i \Delta r$, where Δr are N uniform discretisations $i = 0; 1; \dots; N$, across the domain at t_0 .

3. Calculate the initial masses between nodes using Simpson's Rule $b_i = \int_{r_0}^{r_i} u(r) dr$, between the origin at r_0 , and nodes r_i , for $i = 0; \dots; N$.

Then, at each time step,

1. Calculate the velocities from equation (12), approximating the gradient by suitable finite differences, for example, central differences:

$$\frac{\partial u}{\partial r_i} = \frac{u_{i+1}(t) - u_{i-1}(t)}{r_{i+1}(t) - r_{i-1}(t)} \quad i = 1; \dots; N-1:$$

2. Define the velocity of the final node at r_N through linear extrapolation

$$v_N = 2v_{N-1} - v_{N-2}$$

or by using the one-sided difference

$$v_N = \frac{u_N - u_{N-1}}{r_N - r_{N-1}};$$

3. Update the new positions at the next time step using the explicit Euler scheme

$$r_i(t + \Delta t) = r_i(t) + \Delta t \frac{dr}{dr_i};$$

for equally spaced time steps Δt .

4. Update the solutions at the next time step using the new positions from step 3,

$$u_i(t + \Delta t) = \frac{b_{i+1} - b_{i-1}}{r_i(t + \Delta t)(r_{i+1}(t + \Delta t) - r_{i-1}(t + \Delta t))}; \quad \text{for } i = 1; \dots; N-1:$$

5. Calculate u at the origin by approximating the integral/mass between the origin and the first mesh point at $t + \Delta t$,

$$\int_0^{r_1(t+\Delta t)} u r \, dr = \frac{1}{4} (u_0(t+\Delta t) + u_1(t+\Delta t)) r_1(t+\Delta t)^2 - r_0(t+\Delta t)^2 = b_1:$$

The value of b_1 is constant for all time. Therefore

$$u_0(t+\Delta t) = \frac{4b_1}{r_1(t+\Delta t)^2} - u_1(t+\Delta t)$$

as $r_0(t) = 0$ $\forall t$.

6. Finally, the value of $u_N(t+\Delta t) = \frac{1}{5}u_0(t+\Delta t)$, from the boundary condition at r_N $\forall t$.

Results are presented in Section 4.1.

At r_i , it is assumed that the boundary values are given by the self similar solution $u(r; t) = u(0; t) = 5$. The initial conditions are also taken to be the solutions to the self similar solution at $r_i(t)$. We start with the initial conditions

$$u_i = \frac{2}{5} \quad \text{at} \quad t_0 = 1$$

therefore from equation (8)

$$r_0 = \frac{8}{5} \quad \text{at} \quad t_0 = 1:$$

Also, from the self similar solution, substituting $t_0 = 1$ into the appropriate equations

$$\frac{\partial u}{\partial t_i} = \frac{(r_i)^2}{8} \quad \text{at} \quad t_0;$$

and

$$\frac{\partial u}{\partial r_i} = \frac{r_i}{4} \quad \text{at} \quad t_0:$$

We can also find an expression for the initial velocity of the slow/fast interface, $r_i(t)$, from

$$\frac{du}{dt}_i = \frac{\partial u}{\partial r_i} \cdot \frac{dr}{dt}_i + \frac{\partial u}{\partial t_i} :$$

Since at the interface

$$\frac{du}{dt}_i = 0 \quad \text{at time} \quad t;$$

then the velocity at the interface node is therefore given by

$$\begin{aligned} \frac{dr}{dt}_i &= \frac{\partial u}{\partial t_i} \cdot \frac{\partial u}{\partial r_i} \\ &= \frac{r_i(t)}{2t} \cdot \frac{4}{r_i(t)^2} \quad \text{at} \quad t: \end{aligned} \quad (13)$$

Due to the flux into the region at $r_i(t)$ (from what is the slow diffusion regime)

$$r_i \frac{\partial u}{\partial r} + r_i \frac{dr}{dt} = 0 \quad \text{at} \quad r_i(t):$$

There is an additional boundary condition at $r_N(t)$, that maintains/drives migration

of the liquid.

$$u_b = 0.01 \quad \text{at } r_b; \quad t = 0.$$

The total mass in the fast domain $(r_i(t); r_b(t))$

integrals of u from $r_0(t)$ to $r_i(t)$, where $i = 1 (= 0); 1; \dots; N$

at time t , we obtain

$$\frac{dr}{dt}_i = \frac{u_i r_i}{u_i r_i} (1 - i) \frac{dr}{dt}_i + \frac{(u_i)^m r_i}{u_i r_i} (1 - i) \frac{\partial u}{\partial r_i} (u_i)^{m-1} \frac{\partial u}{\partial r_i} : \quad (19)$$

Hence, calculating the velocity of the internal nodes at any time requires knowledge of the boundary values at r_i , i.e, u_i , $\frac{dr}{dt}_i$ and $\frac{\partial u}{\partial r_i}$, making use of the self similar solution. Using the previous equation (13), to recap

$$\frac{dr}{dt}_i = \frac{r_i}{2t} - \frac{4}{r_i t} \quad \text{at time } t$$

and from our knowledge at the interface,

$$\frac{\partial u}{\partial r_i} = \frac{r_i}{4t} \quad \text{and} \quad \frac{\partial u}{\partial t_i} = \frac{(r_i)^2}{8t^2} - \frac{1}{t^{3/2}};$$

we can substitute these into expressions into equation (19) obtain

$$\frac{dr}{dt}_i = \frac{u_i r_i}{u_i r_i} (1 - i) \frac{r_i}{2t} - \frac{4}{r_i t} + \frac{(u_i)^m r_i}{u_i r_i} (1 - i) \frac{r_i}{4t} (u_i)^{m-1} \frac{\partial u}{\partial r_i} :$$

This is how the velocity of the spatial nodes $r(t)$ progress in the superfast diffusion domain.

We now seek a suitable time-stepping method for the superfast moving mesh method, and update the position of each spatial node by

$$r_i(t + \Delta t) = r_i(t) + \Delta t \frac{dr}{dt}_i ;$$

and the total mass $m_{fast}(t + \Delta t)$ by

$$m_{fast}(t + \Delta t) = m_{fast}(t) + \Delta t \dot{m}_{fast}^0(t);$$

where $\dot{m}_{fast}^0(t)$ is given by equation (15). We have expressions for both $\frac{\partial u}{\partial r_i}$ and $\frac{dr}{dt}_i$ (derived from the self similar solution). So equation (15) becomes

$$\dot{m}_{fast}^0(t) = \frac{(r_i)^2 u_i}{2t} - \frac{(u_i)^{m-1}}{2} - 1 + \frac{4u_i}{r_i t} : \quad (20)$$

We can now recover the solution for $(r(t + \Delta t); t + \Delta t)$ at the next time step, approx-

imating equation (16) as

$$u_i(t + \Delta t) = u_{fast}(t + \Delta t) \frac{r_{i+1}^{i+1} - r_{i-1}^{i-1}}{r_i(t + \Delta t)(r_{i+1}(t + \Delta t) - r_{i-1}(t + \Delta t))}: \quad (21)$$

The individual mass fractions (ϕ_i) do not change with time. The self similar solution is used to calculate values of $u(r; t)$ and the velocities of the spatial nodes x_i at time $t = 0$, at what would be the boundary with the slow diffusion regime.

In the superfast region we can no longer use the self-similar solution, and fit a parabola between the final node of the self similar solution/slow parabola, and the final node in the superfast diffusion profile, where we have assigned a fixed value of $u(N; t) = 0.01$. We give the solution at the final node this small value of u in order to ensure the advancement of the fluid. In reality, where $u(N; t) = 0$ the capillary bridges in Figure 3 would collapse and no longer exist, and therefore there would be no further

The initial values of $u_i(t_0)$ in the fast diffusion regime are given by

$$u_i = u_N + (u_I - u_N) \frac{N - r + r_I - r_i}{(N - r)^2} : \quad (22)$$

The total mass in the fast region, att_0 is therefo

3. Define the boundary conditions at $r_i(t)$ at time t

$$u_i = \frac{2}{\rho} \frac{r_i}{t}; \quad \text{as given by the self similar solution}$$

$$v_i = \frac{r_i}{2t} - \frac{4}{r_i} \frac{1}{\rho t}; \quad \text{as given by the self similar solution}$$

4. Define the boundary conditions at $r_b(t)$

$$u_b$$

4. Compute the new total mass from $m_I(t + \Delta t)$ to $m_N(t + \Delta t)$ using $\dot{m}_{fast}^0(t)$ calculated from Equation (20), and explicit Euler method.

$$m_{fast}(t + \Delta t) = m_{fast}(t) + (\dot{m}_{fast}^0(t)) \Delta t$$

The boundary conditions at $r_0 = 0$, $t_0 = 1$ are

$$\begin{aligned} u_0 &= 2; \\ \frac{\partial u}{\partial r_0} &= 0; \\ \frac{dr}{dt}_0 &= 0; \end{aligned}$$

and for all time $t > 0$,

$$\frac{\partial u}{\partial r_0} = 0;; \quad (23)$$

$$\frac{dr}{dt}_0 = 0;; \quad (24)$$

as, intuitively, the origin about which diffusion is symmetric, $r_0(t)=0$.

Let us denote the position and solution at the interface between slow and superfast diffusion as r_I and u_I respectively, at t_0 , where I is the spatial nodal identity. We know from previous equations (25), (26), (27), and (28) respectively, that at $t_0 = 1$ for an initial discretisation $r = \frac{1}{4^p 5}$,

$$r_I = \frac{8}{5}; \quad (25)$$

$$\frac{\partial u}{\partial r_I} = \frac{2}{5}; \quad (26)$$

$$\frac{dr}{dt}_I = \frac{3^p 5}{10}; \quad (27)$$

$$\frac{\partial u}{\partial t_I} = \frac{3}{5}; \quad (28)$$

Howl.8)

Therefore, since

$$\frac{dr}{dt}_0 = 0 \quad \text{and} \quad \frac{\partial u}{\partial r_0} = 0 \quad \text{at} \quad r_0(t) = 0$$

$$\frac{dr}{dt}_i = \frac{u_i r_{i-1}}{u_i r_i} \quad @u$$

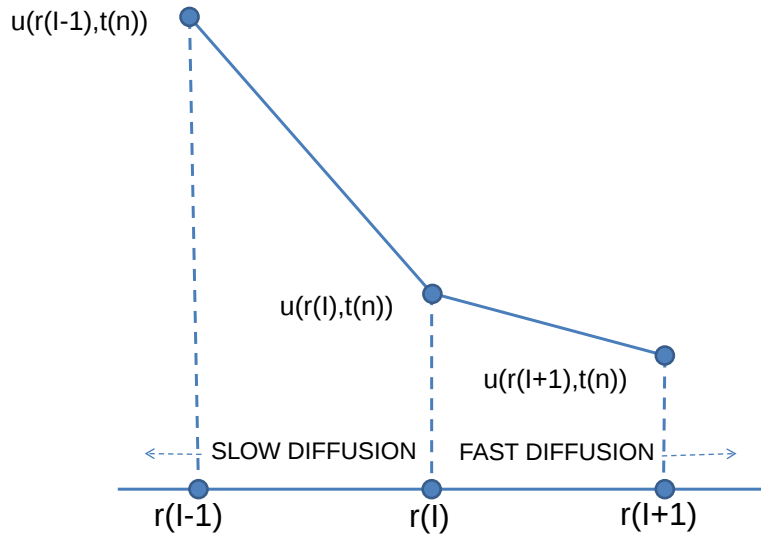


Figure 6: Identification of velocity of interface node between slow and fast diffusion regimes

There will be zero rate of change of mass as mass flows at the same rate into the superfast regime as flows out of the slow regime, by the application of the continuity equation at the boundary;

$$\frac{d}{dt} \frac{1}{\text{slow}(1)} \int_{r_{l-1}(t)}^{r_l(t)} u r dr + \frac{1}{\text{fast}(1)} \int_{r_l(t)}^{r_{l+1}(t)} u r dr = 0: \quad (31)$$

where $\text{slow}(1)$ and $\text{fast}(1)$ represent the total mass in the slow and fast regimes respectively at time t_0 . The integral to the left of the boundary is given by

$$\frac{d}{dt} \frac{1}{\text{slow}(1)} \int_{r_{l-1}}^{r_l} u r dr = \frac{1}{\text{slow}(1)} \int_{r_{l-1}}^{r_l} \frac{\partial u}{\partial t} r dr + u r \frac{dr}{dt} \Big|_{l-1}^{l} + \frac{1}{(\text{slow}(1))^2} \frac{d \text{slow}(1)}{dt} \int_{r_{l-1}}^{r_l} u r dr; \quad (32)$$

an to t r t t s

$$\overline{t}^1$$

where

$$A = \frac{u_l r_l}{\text{slow}(1)} 1_{l=1} - \frac{(r_l^2 - r_{l-1}^2)(u_l + u_{l-1})}{4 \text{slow}(1)} \\ + \frac{u_l^m r_l}{\text{fast}(1)} - \frac{(r_{l+1}^2 - r_l^2)(u_{l+1} + u_l)}{4 \text{fast}(1)} 1_{l+1}$$

and

$$B = \frac{u_l r_l}{\text{slow}(1)} 1_{l=1} - \frac{(r_l^2 - r_{l-1}^2)(u_l + u_{l-1})}{4 \text{slow}(1)} \\ + \frac{u_l r_l}{\text{fast}(1)} - \frac{(r_{l+1}^2 - r_l^2)(u_{l+1} + u_l)}{4 \text{fast}(1)} 1_{l+1}$$

7. Combining the initial profile for slow and fast dispersive regimes at initial time t_0 .

Now that we have expressions for the velocity of the spatial non-singular solution, we can write the equation for the supercritical equation $\tilde{u} = \phi$ on

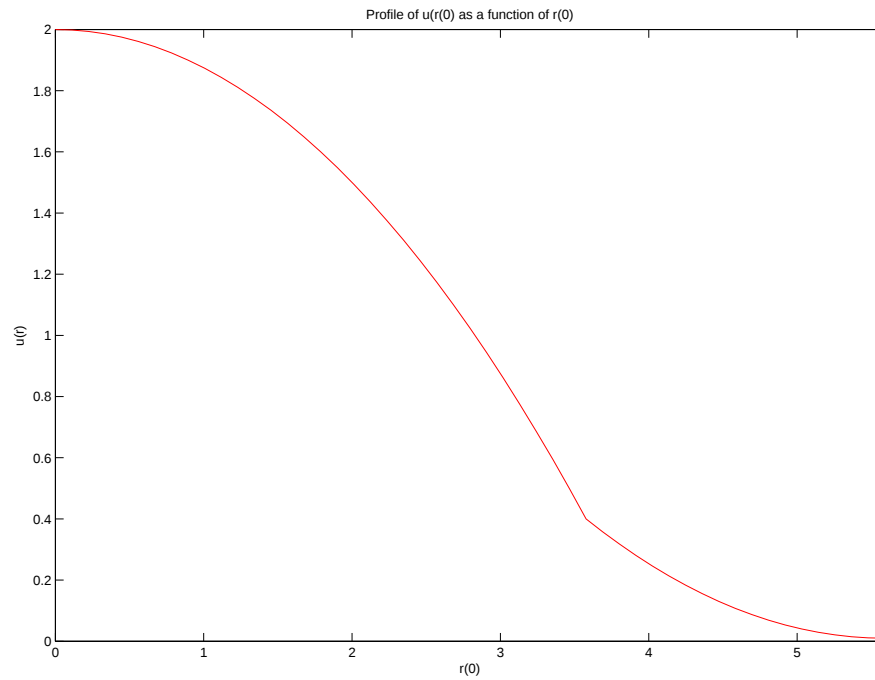


Figure 7: Combined slow and fast diffusion profiles at t_0 .

7. Generating an algorithm for the combined diffusion.

Now we return to a variant of the problem.

Combining slow and superfast diffusion

For a set $r_i, i = 0, \dots, N$

$$0 = r_0(t) < r_1(t) < \dots < r_{N-1}(t) < r_N(t)$$

with $r_N(t) = 1$ at t_0 with N nodes separated by $r_N(t)$ in a domain Ω . Let $r_1(t)$ be the first node at which the slow diffusion starts.

In this

At t_0 an initial condition

$$u_N(t) = 0.01;$$

C a u a t t v o t

From the above relation the solution for the spatial coordinate is a constant

$$u_N(t+\tau)=0.01$$

Calculate the solution at the origin r_0

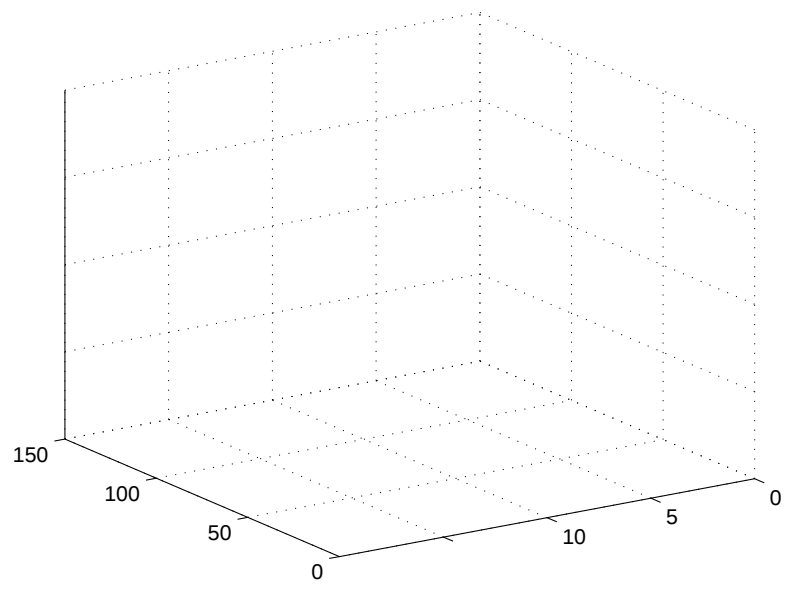
$$u_0(t+\tau)=\frac{4_{slow}(t+\tau)-1}{(r_2(t+\tau))^2}u_1(t+\tau);$$

as a function of time

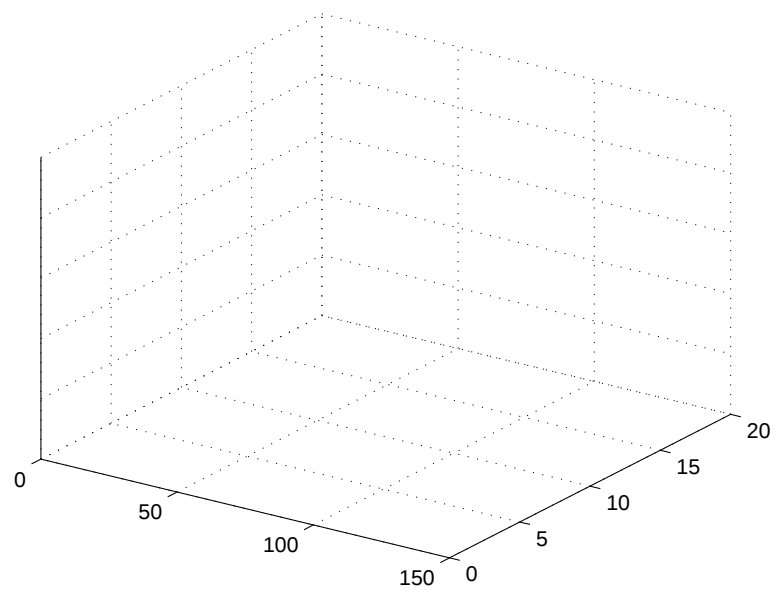
Calculate the input solution at the interface

$$u_l(t+\tau)=u_{in}$$

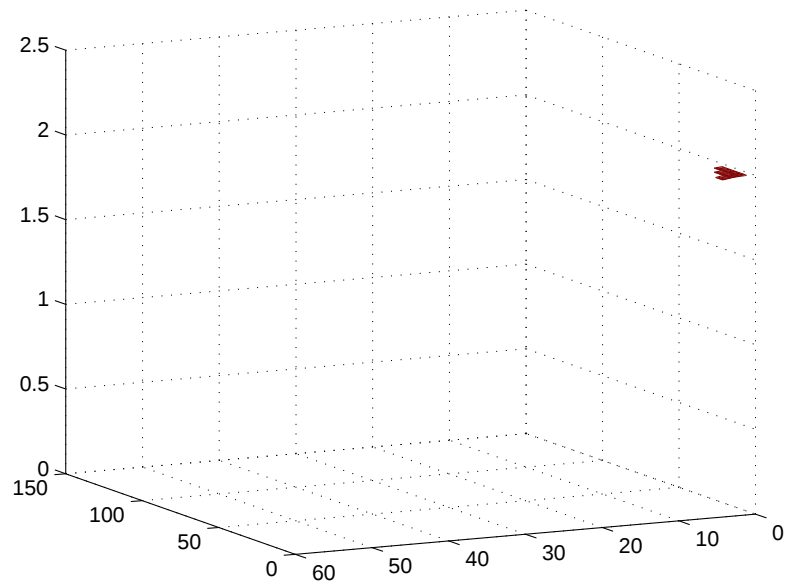
4 Results

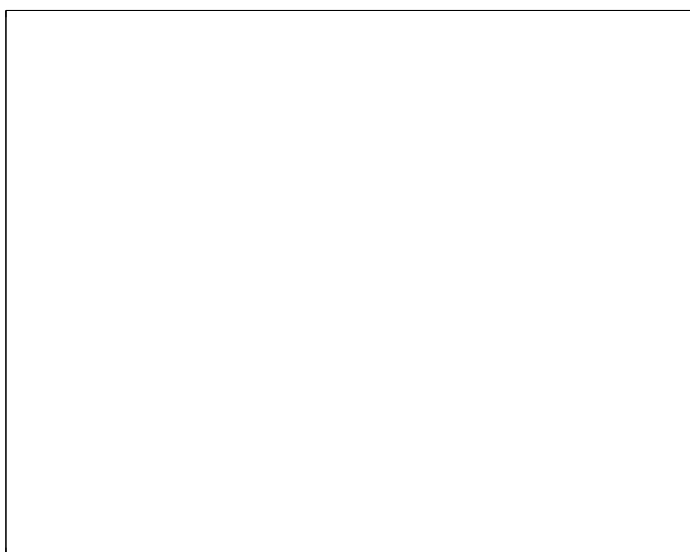


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For $\vec{v}$ vote so that no s has w_t n as n t and t v o t
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 and a on pro o t as s r n r r n





on t r s o t nt r a

$$\frac{\frac{\partial u}{\partial r_l}}{\frac{\partial u}{\partial r_l}} = \frac{u_l}{r_l} - \frac{u_{l-1}}{r_{l-1}} \text{ on slow us on s o nt r a}$$

an

$$\frac{\partial u}{\partial r}$$

5 Discussion and Conclusions

In this section we discuss the predictions and conclusions resulting

from the present analysis. The numerical results show that the porous medium is a two-dimensional system and the flow is laminar. The non-Newtonian behavior is characterized by the power-law index n and the consistency index K . The results show that the flow is laminar and the power-law index n is greater than 1. The consistency index K is determined by the material properties. The results show that the flow is laminar and the power-law index n is greater than 1. The consistency index K is determined by the material properties. The results show that the flow is laminar and the power-law index n is greater than 1. The consistency index K is determined by the material properties.

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strain rate required to attain a stress of 50 MPa is shown in Fig. 1. For steady state conditions, the required time at $T < 5 \times 10^{-5}$ s is too short to allow for the CF contribution.

In the steady state value of $u_1(t)$ at the time of annealing, the value of $u_1(t)$ was

6 Recommendations for future work

rou out t ours o t s stu w av a a nu r o assu pt ons on
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n u a **number** o nt r a s sa $i = 1_1; 1_2; ::; 1_R$ or R an s n m As n t
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Yost F G an oo E J Capillary ow in irregular surface
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§ Ba n s J Hu ar E an J a ¶ A moving mesh nite element
algorithm for the adaptive solution of time dependent partial di erential equations
with moving boundariesCo un Co put s

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tions s on Ca r n v rs t r ss Ca r

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s an ¶ MSc Thesis: Numerical schemes for a non-linear di usion problem
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rn J MSc Thesis: Fast diffusion through porous media n v r s t o a
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Bar n att G I Scaling Ca r n v r s t r s s Ca r

Ba n s J an E A large time-step implicit moving mesh scheme for
moving boundary problems u t o s or art a D r nt a Equat ons

n r G F an Gra G Finite element simulation in surface and subsur-
face hydrology A a r s s w Yor